

Case Study: Development and Scale-up of a Helper-Dependent Adenovirus (HDAd) Process Using the iCELLis[®] Bioreactor Platform

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INTRODUCTION

Viral vectors are currently the preferred gene-delivery vehicle for most cell and gene therapies, and clinical trials require high titer virus preparations to adequately deliver the therapeutic transgenes to clinical subjects or target cells. For this reason, technologies that enable the industrialization of these processes in a safe, robust, and cost-effective way are necessary to support the demands of the patient population. However, complexity around developing and scaling viral vector processes to commercial manufacturing scale, and the lack of standardized approaches remain as challenges that can impact therapy development timelines and productivity. Selection of the appropriate production platform plays a key role on the successful implementation of a process that meets the commercialization timelines and manufacturing costs. We will share a case study that demonstrates the successful steps taken to develop and scale up a customer process for a HDAd, leveraging Pall's process expertise and the iCELLis bioreactor platform, to help accelerate the development timelines. Critical process parameters for development and manufacturing, such as seeding density, infection density, and harvest strategy, were first tested at the flatware stage, and continually optimized over the course of the iCELLis Nano bioreactor development stage. The optimized parameters were used successfully in duplicate scale-up batches at the iCELLis 500+ bioreactor scale to demonstrate a process ready for tech transfer.

RESULTS

Seeding Density Screening to Reduce Seed Train Burden



Development Parameters Scaled Successfully to iCELLis 500+ Bioreactor



Adherent Process Production Scale Options Yielding Same Surface Area





- Lower seeding density and extended growth duration screened in flatware
- Reduced seed density to 4.5 x 10³ cells/cm² to minimize required number of N-1 passage vessels
- Target infection density increased to 2–3 x 10⁵ cells/cm² in the iCELLis Nano Bioreactor

| Seeding Density (vc/cm²) | 4,500 | 7,000 | 28,000 |
|---|-------|-------|--------|
| Growth post-inoculation (days) | 8 | 7 | 4 |
| CellSTACK•10 layers required to inoculate 333 m² iCELLis 500+ Bioreactor | 14 | 22 | 86 |

Lysis Process Modified for Manufacturability and **Reduced Step Duration**



Figure 6

Cell growth profile (iCELLis Nano bioreactor carrier counts vs iCELLis 500+ bioreactor biomass probe)



Side-by-side iCELLis Nano and 500+ bioreactors using optimized process parameters yielded similar metabolite and cell growth profiles (N=2)

1960 x Roller Bottles







Improved Manufacturability and Process Flexibility Throughout Development

Figure 7

HDAd titer during process development workflow



- Significant increase in productivity compared to flatware production
- Productivity of iCELLis Nano and iCELLis 500+ bioreactors were comparable

CONCLUSIONS

The process was successfully optimized for scalability and manufacturability in the iCELLis Nano bioreactor then scaled to the iCELLis 500+ bioreactor. Screening studies in flatware and several development runs in the iCELLis Nano bioreactor led to a simplified seed train, identification of an efficient lysis buffer resulting in reduced lysis time, and a decrease in the harvest volume to be processed during downstream processing. The process demonstrated improved productivity compared to the flatware process and comparable virus productivity, cell growth and metabolite trends between the bioreactor scales. This data demonstrates that a scalable, manufacturing process for HDAd can be successfully developed using the iCELLis Nano bioreactor then scaled to commercial manufacturing scale using the iCELLis 500+ bioreactor.

MATERIALS & METHODS

- Host cell line: HEK293
- Base medium:
- MEM + FBS + glucose + glutamine
- Virus: HDAd, Helper virus

Lysis buffer: Buffered surfactant Rinse buffer: 10 mM Tris HCl

Nuclease: Benzonase*

Flatware Screening to Provide Confidence in Range of Parameters to **Test in iCELLis Nano Bioreactor**

| Tech Transfer and Screening | Co-Infection Optimization |
|--|---|
| Reproduce results at Pall Process Development Services (PDS) labs | Define acceptable infection density range |
| Screen seeding density and define cell growth rate | Screen cell lysis reagents select one for future use |
| Define passage cadence and growth duration | Establish minimum cell lysis duration |
| Define media ratio and cell dissociation volumes | |

Optimization and Scale-Up Parameters in iCELLis Bioreactors



in iCELLis Nano

bioreactor



- Maximal virus recovery achieved after 2 hour lysis time
- Reduced lysis time enables same day harvest clarification process

Virus Recovery Improved with Rinse Implementation



| iCELLis Nano Bioreactor Dev. Round #1 | ELLis Nano Bioreactor Dev. Round #2/3 | ELLis 500+ Bioreactor Engineering | | |
|--|---|--------------------------------------|---|---|
| Seeding density Infection time Multiplicity of infection (MOI) | Seeding density Infection density Media ratios Multiplicity of Compaction Lysis Method Obtain comparable results at scale Parallel iCELLis Nano bioreactor control | | Figure 4 Harvest strategy screening Spent Media Binse | |
| Parameters | iCELLis Nano Bioreactor | iCELLis 500+ Bioreactor | Lysate | |
| Fixed-bed size (m²) | 0.53 – 4.00 | 333 | | Ţ |
| Growth medium ratio (mL/cm²) | 0.23 | 0.23 | | |
| Infection medium ratio (mL/cm²) | 0.16 – 0.23 | 0.16 | | |
| Infection cell density (x10 ⁵ vc/cm ²) | 2.1 – 2.7 | 2.6 – 2.7 | | |
| Recirculation loop volume (L) | 1.2 – 6.4 | 700 | - Nogligiblo virus in | |
| MOI | Constant | | Decirculation media | |
| Lysate and rinse buffer volumes | Vessel working volume | | Fixed-hed rince im | |

supernatant prior to lysis not harvested: 87% reduced harvest volume nproves recovery about 20%

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